

# 2018 UK-China Workshop on Water-wise cities and smart water systems

## Removal of Emerging Contaminants from aqueous solution by a novel Electro-Peroxone-ACF (EOA) process

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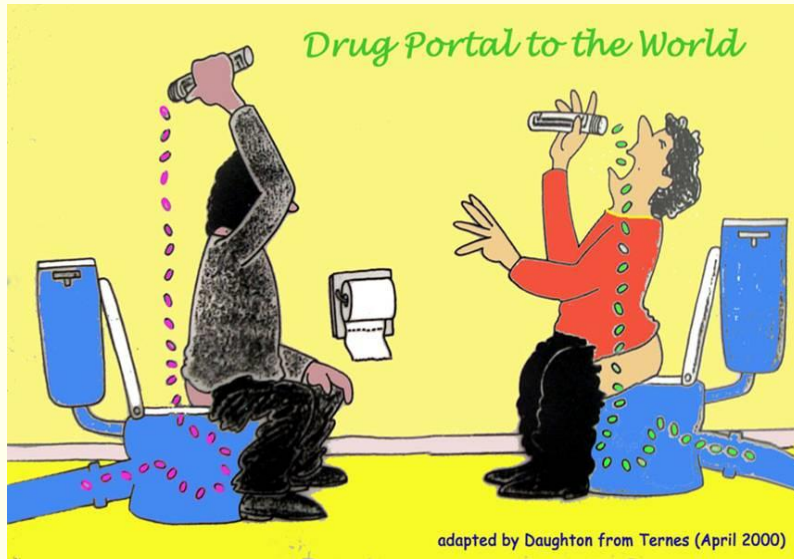
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# Outline

- 1. Back ground**
- 2. Research contents**
- 3. Result and discusstion**
- 4. Summary**

# Emerging Contaminants (ECs)



The pollution of water by “**Emerging Contaminants**” has become a major global environmental problem.

ECs such as **perfluorochemical (PFOS)**, **endocrine disruptors (EDCs)**, **pharmaceuticals** and **personal care products (PPCPs)**, **polycyclic aromatic hydrocarbons (PAHs)** and **brominated flame retardants (BFR)** are constantly discharged into the water environment.

# Risk of Emerging Contaminants

Toxicological studies show that ECs are of chronic toxicity to microorganisms, amphibians and fish even at trace levels of concentration.

Conventional water treatment can not effectively remove ECs.

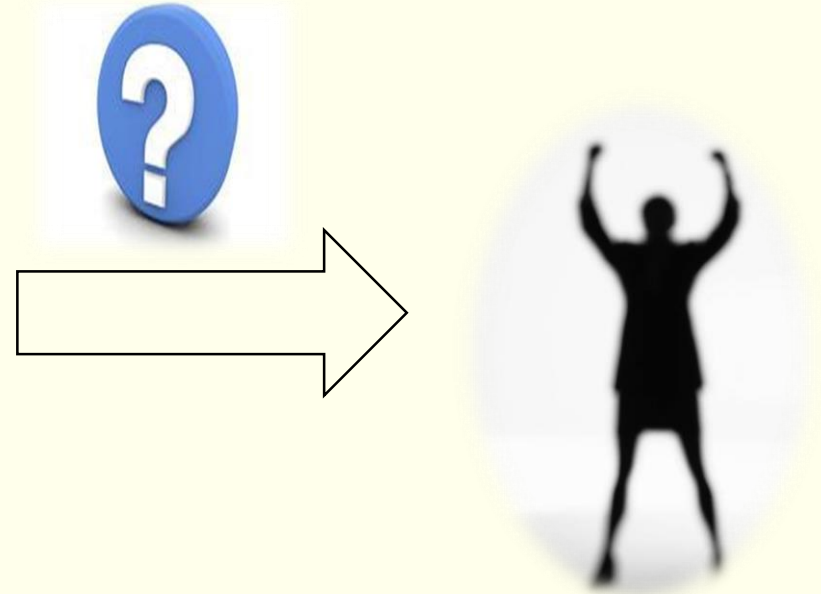
**Thus, it is urgent to develop novel water treatment technologies for removing ECs from water with high efficiency and low consumption.**

Daughton, C.G., et al. International Encyclopedia of Public Health. 2017: Academic Press. 66. C.S.G.

Ferreira, et al., Ecotoxicol. Environ. Saf. 67 (2018), pp. 452.



# The potential harm for human



[http://www.nsf.gov/news/news\\_summ.jsp?cntn\\_id=123689&WT.mc\\_id=USNSF\\_51&WT.mc\\_ev=click](http://www.nsf.gov/news/news_summ.jsp?cntn_id=123689&WT.mc_id=USNSF_51&WT.mc_ev=click)

Jeanne et al. found greatly reduced sperm viability caused by **Tetracycline** had passed from father to son in **pseudoscorpions** by **inheritance**. They suggest a similar effect could occur in humans and other species.

(Jeanne A. Zeh et al. [Scientific Reports, 2012](#))



# Research Progress on Removing ECs from Water

Currently, biological method, membrane filtration, and physicochemical methods are applied for ECs removal.

| Methods                  | Removal Effect | Advantage        | Disadvantage                 |
|--------------------------|----------------|------------------|------------------------------|
| Biological method        | unsatisfactory | Low cost         | Poor stability               |
| Membrane filtration (RO) | Fairly well    | effective        | Fouling and high cost        |
| Physical adsorption      | fair           | Simple operation | Difficult to regenerate      |
| Chemical oxidation       | fair           | Running steadily | High cost and low efficiency |

[1] Yang X, Flowers R C, Weinberg H S, et al. Water Research. 2015, 45(16): 5218-5228.

[2] Liu Z, Ogejo J A, Pruden A, et al.. Science of The Total Environment. 2016, 409(24): 5149-5161.

[3] Chen H, Li X J, Zhu S C. Environmental Science and Pollution Research. 2017, 19(6): 2381-2389.

[4] Esplugas S, Bila D M, Krause L G T, et al. Journal of Hazardous Materials. 2017, 149(3): 631-642.

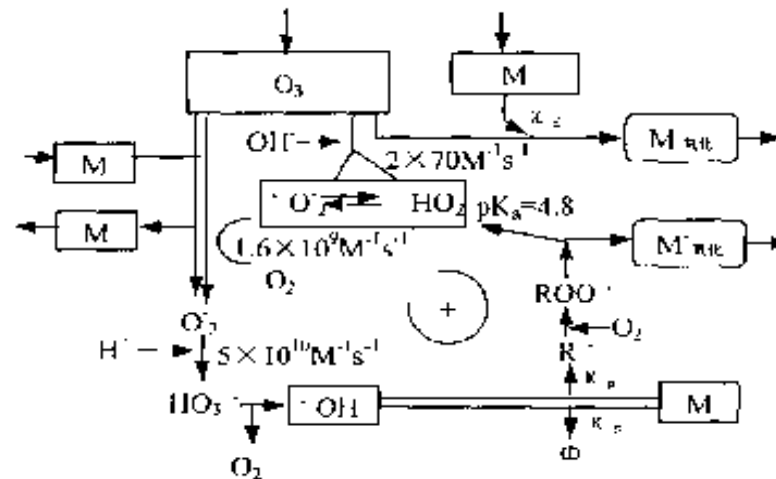
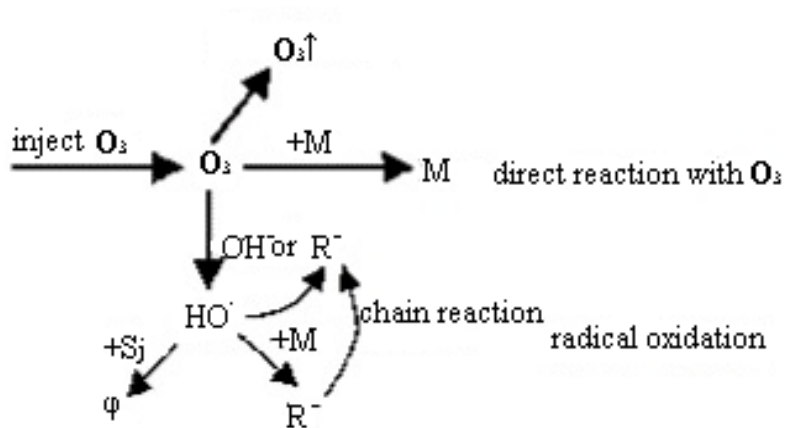
# Research Progress on Ozonation

## Direct reaction:

Organic pollutants +  $O_3$  ( $E_0=2.08V$ )  $\rightarrow$  product or intermediate products; **low speed and selective oxidation**

## Indirect reaction:

Organic pollutants +  $HO\cdot$   $\rightarrow$  intermediate products or  $CO_2+H_2O$   
**higher oxidation potential and react speed without selectivity for most of organic compounds;  $HO\cdot$  ( $E_0=2.80V$ )**



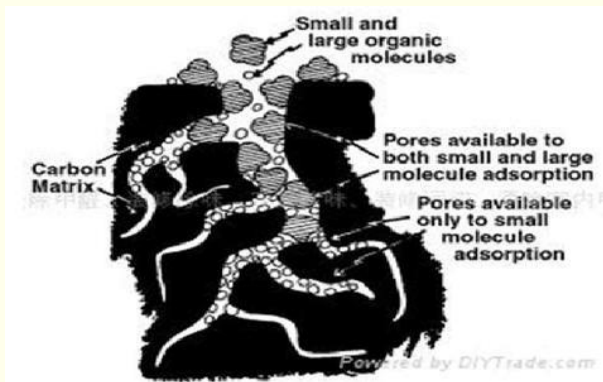
J. Hoigné, et.al. Water Res. 17 (1983) 173-183.

J. Nawrocki, et. al. Appl Catal B-Environ. 99 (2010) 27-42.

# Research Progress on Ozonation

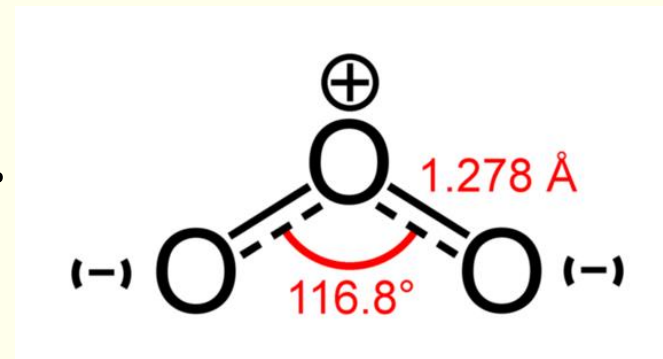
**Indirect reaction: (homogeneous and heterogeneous catalysis of ozone)**

$O_3/Fe^{2+}$ ,  $O_3/Cu^{2+}$ ,  $O_3/UVA$ ,  $O_3/Fe^{2+}/UVA$ ,  $O_3/H_2O_2$ ,  $O_3/AC$ ,  
 $O_3/MnO_2$ ,  $O_3/TiO_2$ , etc.



**AC**

+



**ozone**

M. Sánchez-Polo, U. von Gunten, J. Rivera-Utrilla, Water Res. 39 (2005) 3189-3198.

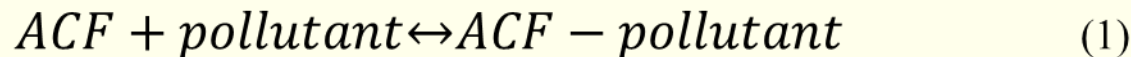
P.M. Álvarez, J.F. García-Araya, F.J. Beltrán, I. Giráldez, J. Jaramillo, V. Gómez-Serrano, Carbon. 44 (2006) 3102-3112.



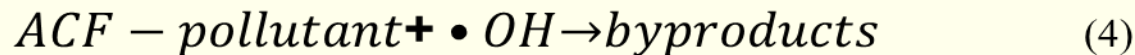
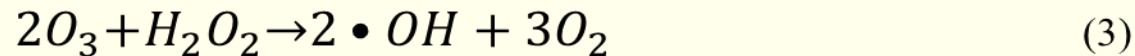
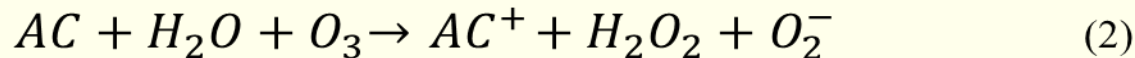
# Research Progress on Ozonation

## ✓ Advantages:

### 1) Rapid adsorption of trace organic pollutants



### 2) Hydrogen peroxide is generated by the reaction of AC and O<sub>3</sub>, which then acts with O<sub>3</sub> to generate hydroxyl radicals



### 3) AC is a green “catalyst” without risk of heavy metal leaking

# Research Progress on Ozonation

## × Disadvantages:

- 1) Relatively low efficiency.
- 2) AC served as an initiator/a promoter but not as a catalyst in AC-peroxone process.
- 3) AC-peroxone process alter the surface morphologies and surface functional groups of AC.

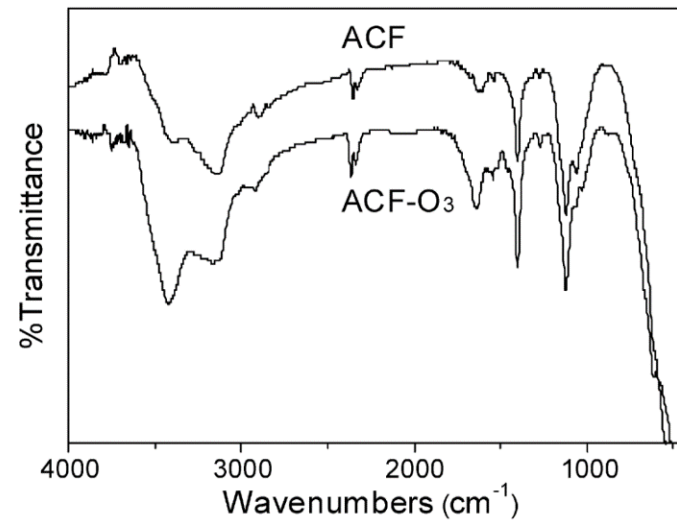
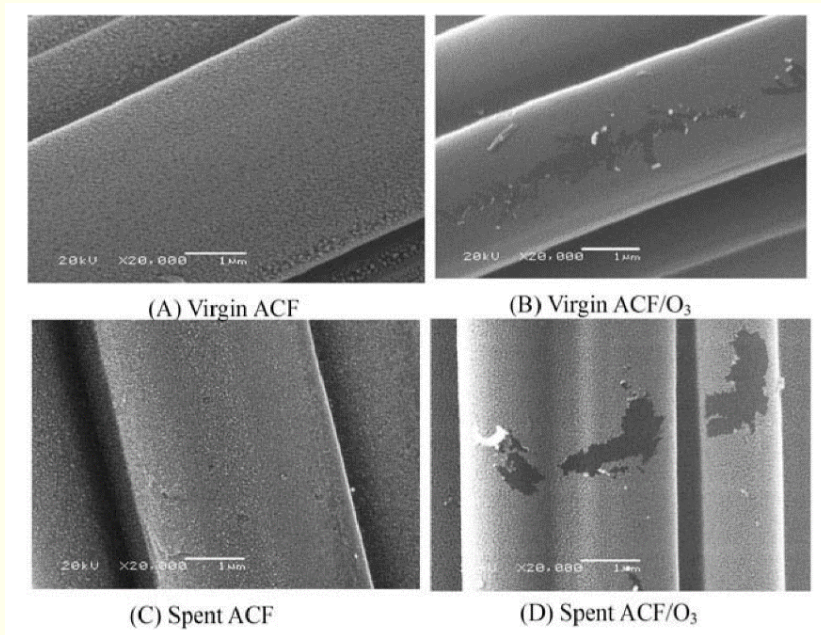
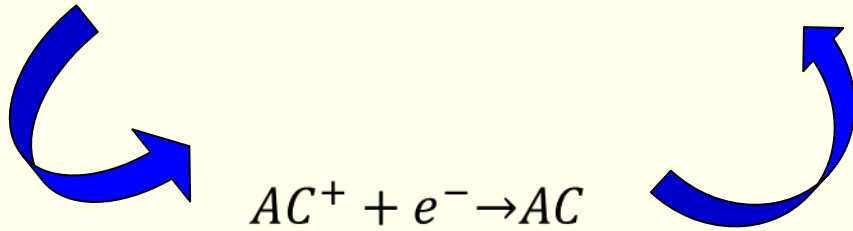
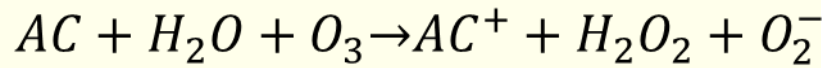


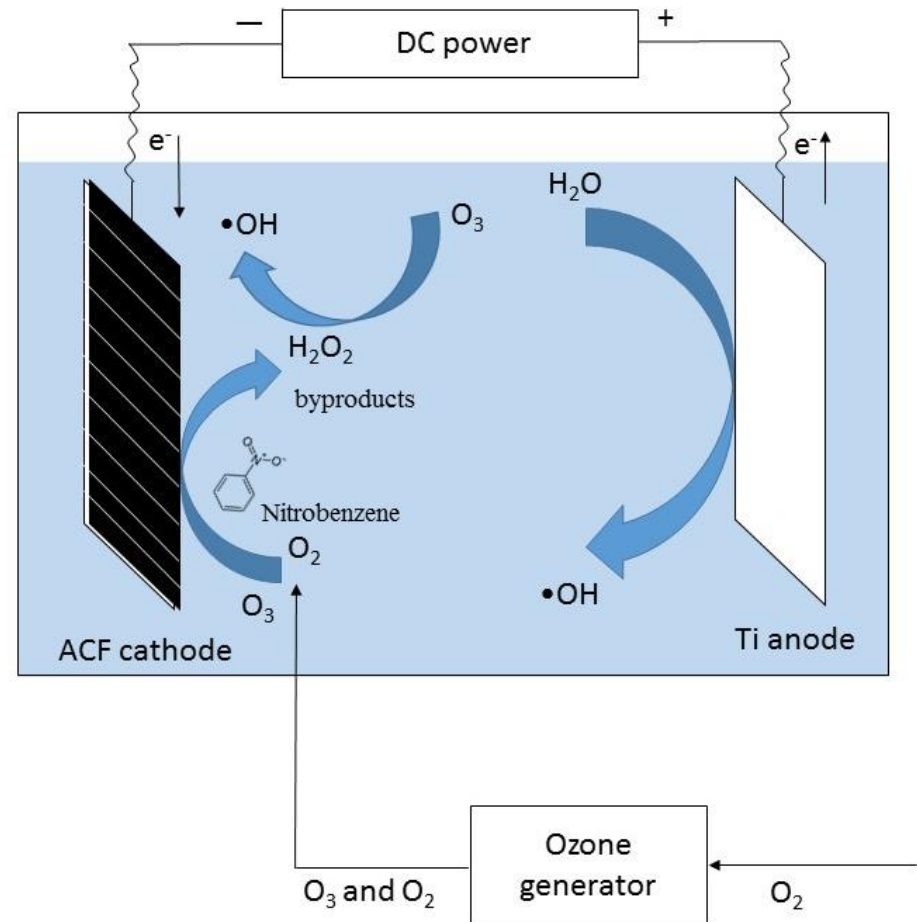
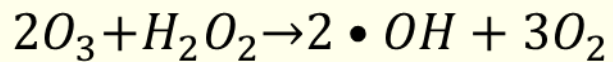
Fig. 6. FTIR spectra of virgin ACF and ACF exhausted after ozonation.

# Research contents

## Theoretical hypothesis:



## Inject electron onto ACF



# Research contents

## Target pollutant—nitrobenzene (NB)

### ✓ Source

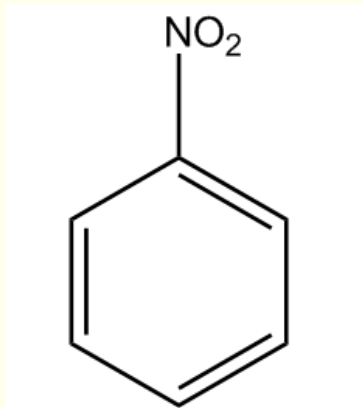
Industrial wastewater of printing , pharmacy, petrochemical engineering, etc.

### ✓ Character and distribution

Stability of Structures, hydrophobic, refractory, and widespread.

### ✓ Toxicity

Oxidation or complexation with hemoglobin, causes acute intoxication, accompanied with nausea, vomiting, headache and other symptoms.



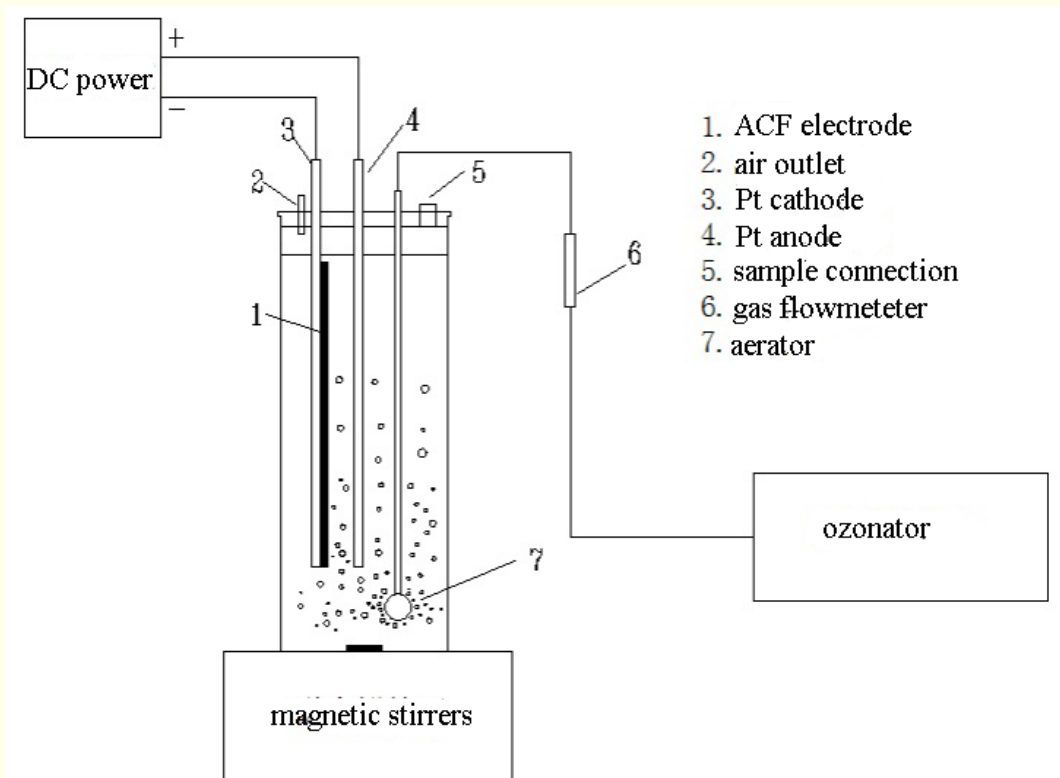
structural formula of NB



NB contamination of Song hua river in 2005

# Research contents

## Reactor design



★ Reactor size :

High: 15cm, Diameter: 7cm

★ Concentration and volume of NB:

12mg/L, 500mL

★ Plate electrode size:

3.5cm × 10cm

★ The way of sampling:

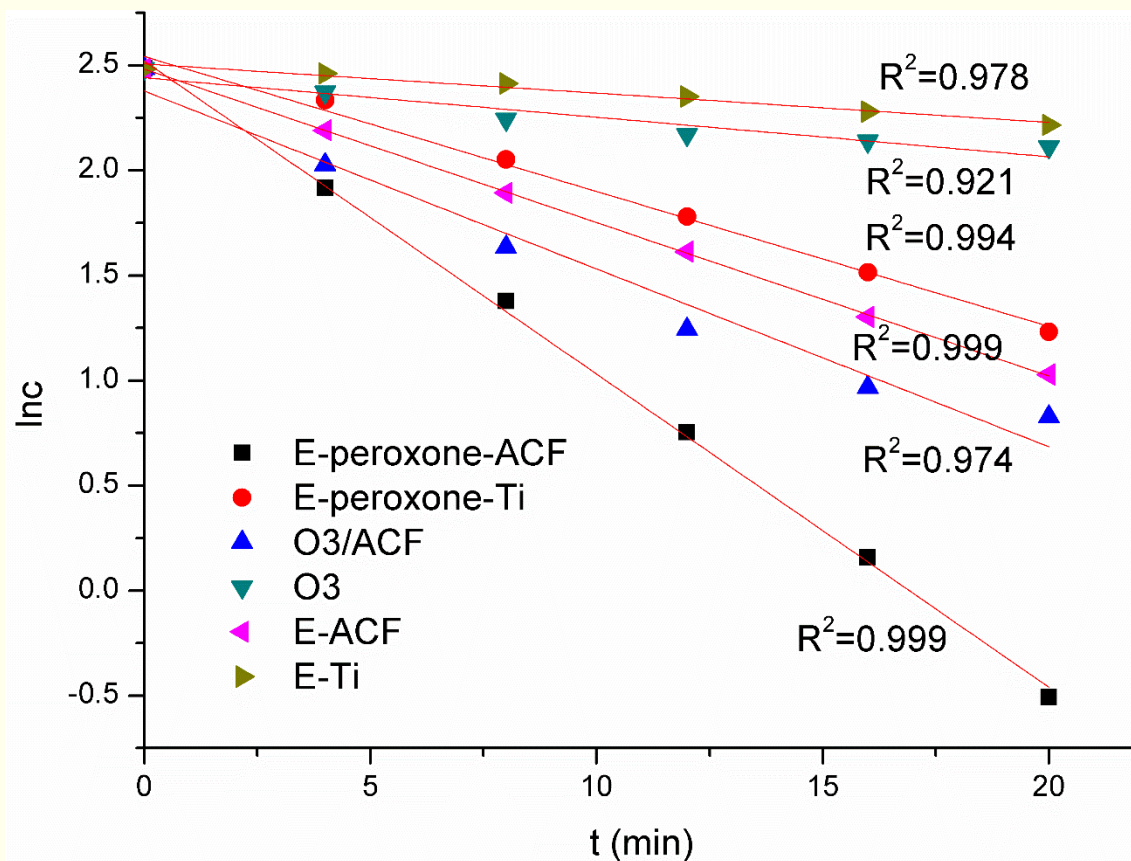
Interval 4 min

★ Test method :

HPLC

# Result and discussion

## Kinetic analyses of NB removal



1 All processes follows pseudo-first-order kinetics, the removal efficiency of EOA is much higher than the others.

2 NB can hardly removed by ozone alone and electricity alone.

3 NB can removed by E-ACF process with a high speed may due to the high absorption ability of ACF.

**4 There is a coupling effect between ozone, ACF, and electrolysis.**



# Result and discussion

## Recycle experiments

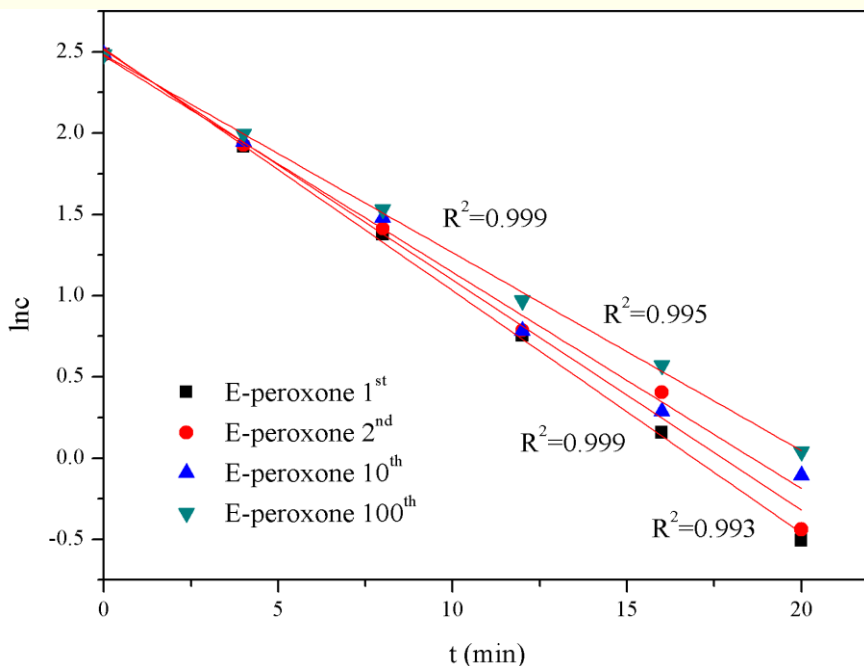


Fig. (a) ACF recycle in E-peroxone-ACF process

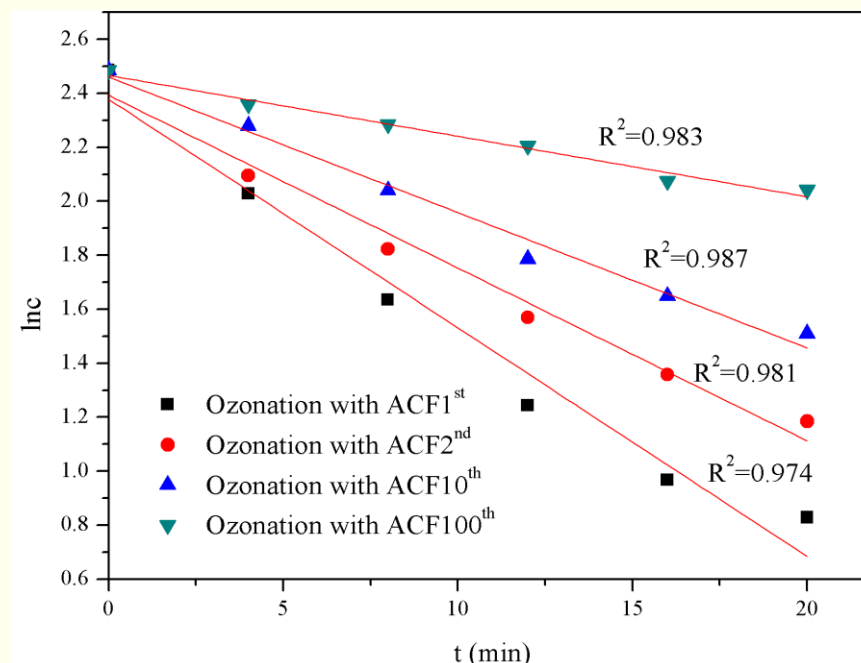


Fig. (b) ACF recycle ACF/ $O_3$  process

- 1、 In EOA process, ACF can maintain the activity even after 100 times recycle. ( $K_{app}$  decreased slowly from  $14.90 \times 10^{-2} \text{ min}^{-1}$  to  $12.18 \times 10^{-2} \text{ min}^{-1}$ )**
- 2、 In OA process, ACF almost lost activity after 10 times recycle.**

# Result and discussion

## Adsorption

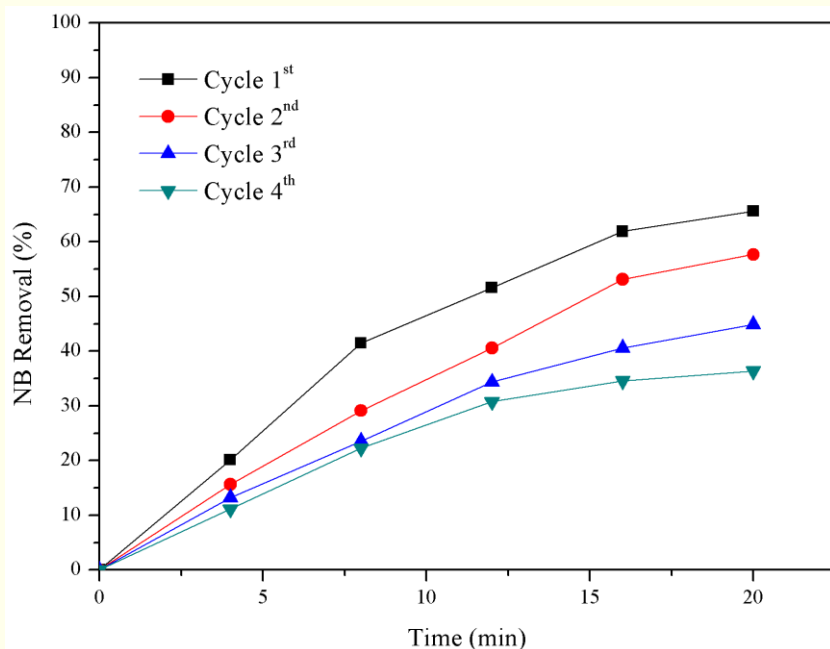


Fig. (a) Removal of NB by ACF for 4 times recycle

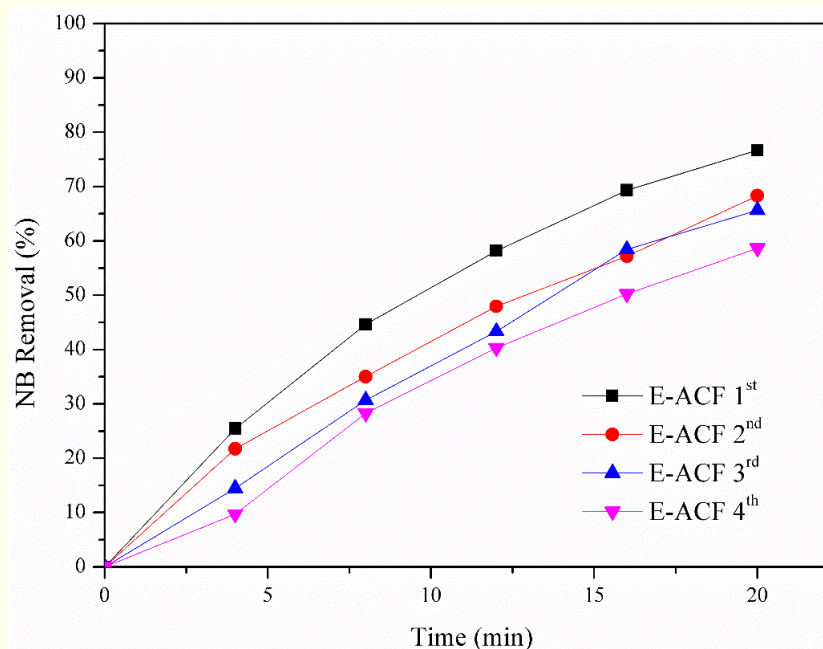


Fig. (b) Removal of NB by E-ACF for 4 times recycle

**1. ACF has a large adsorption capacity for NB, and the adsorption of NB decreases obviously with increasing the recycle times.**

**2. The cathode electric field has little influence on the adsorption of NB by ACF (Fig.(b)).**

# Result and discussion

## Effect of current density and ozone concentration

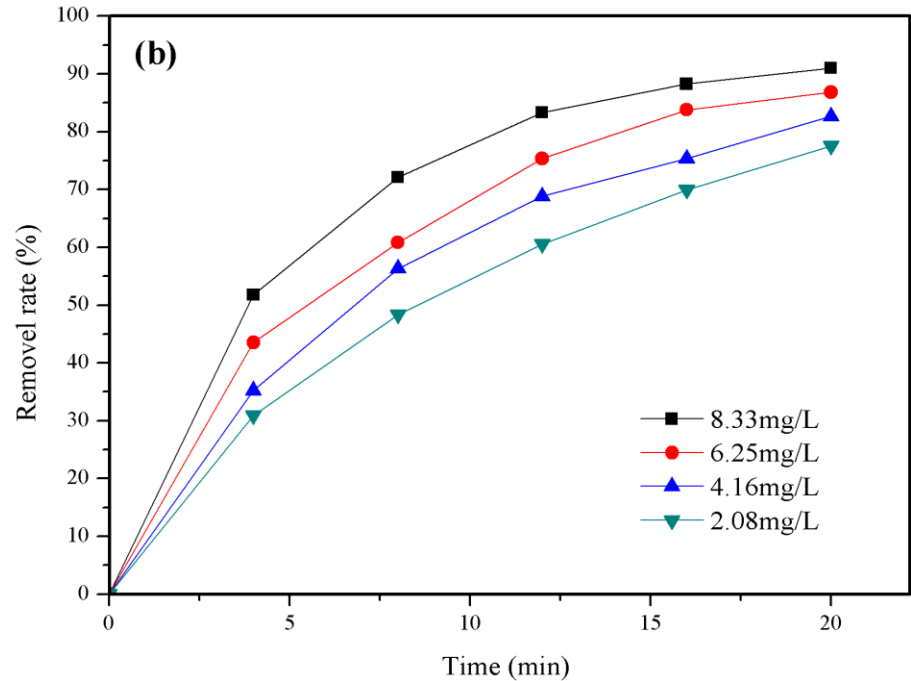
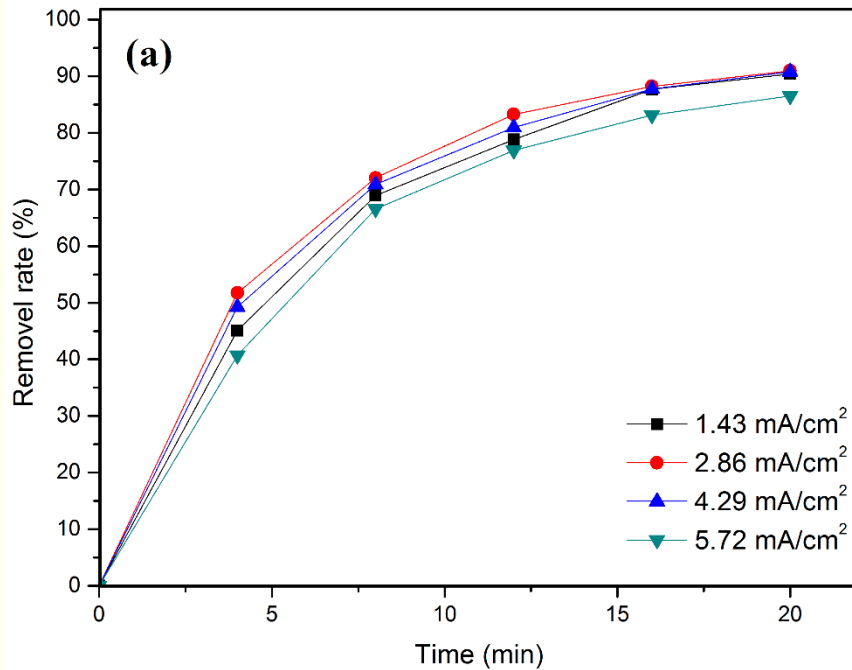


Fig. (a) Effect of current density on E-peroxone-ACF process Fig. (b) Effect of O<sub>3</sub> concentration on E-peroxone-ACF process

1、 As shown in fig. (a), the **optimum current intensity** of NB degradation is **2.86 mA/cm<sup>2</sup>**. Massive generation of hydrogen peroxide ( a kind of hydroxyl radical scavenger ) could lead to the decrease of NB removal efficiency.

2、 Excessive amount of hydrogen peroxide indicates that insufficient of ozone, so **increasing the ozone concentration further increases the NB degradation efficiency** (fig. (b)).

# Result and discussion

## Effect of initial pH

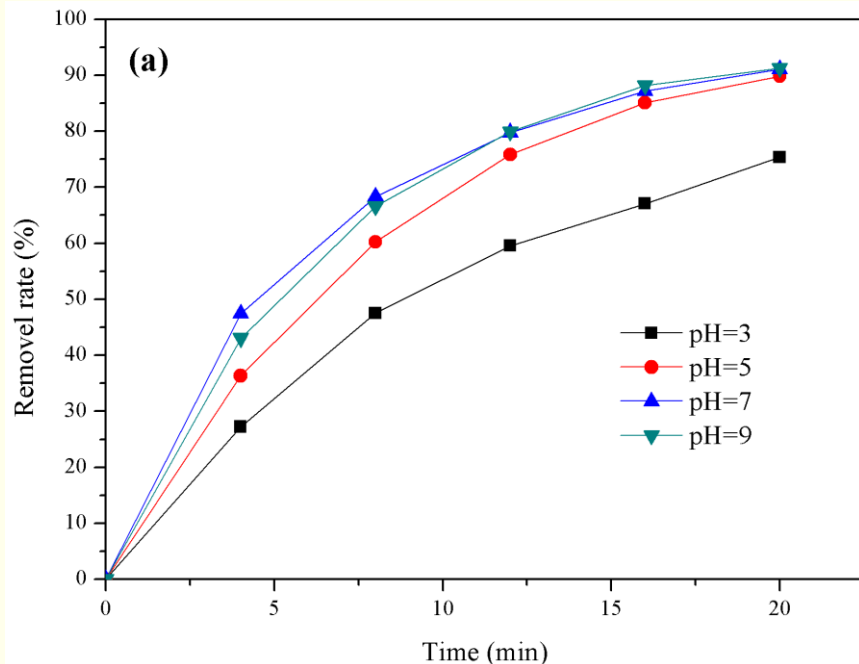


Fig. (a) Effect of pH on ACF/O<sub>3</sub> process

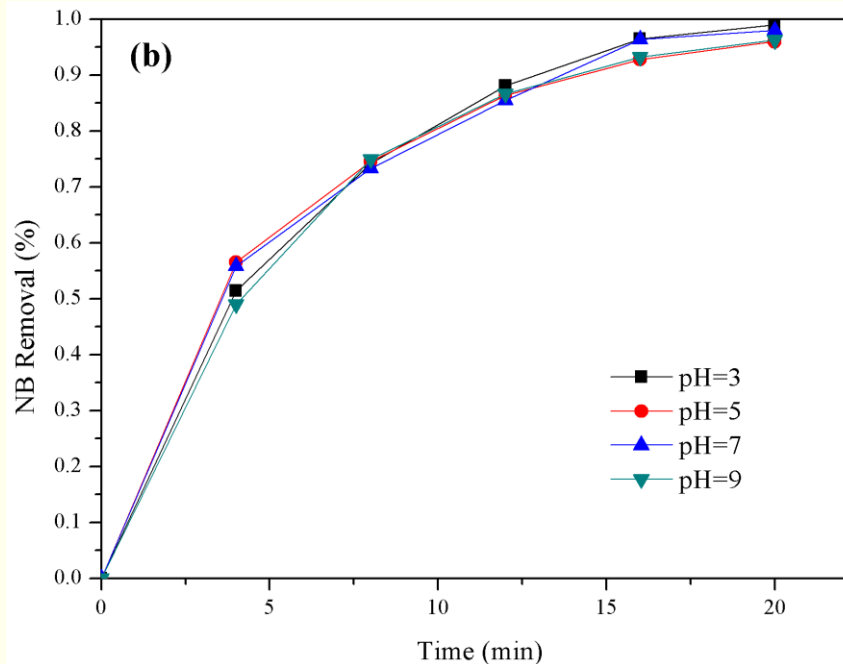


Fig. (a) Effect of pH on E-peroxone-ACF process

1. The initial pH of solution had great influence on O<sub>3</sub>/ACF system (Fig.(a)). NB removal efficiency increased with the elevate of pH value due to hydroxide ion could promote the decompose of ozone.

**2. Initial pH had little impact on removal rate of NB in EOA process.**

# Result and discussion

## Hydrogen peroxide concentration during reaction

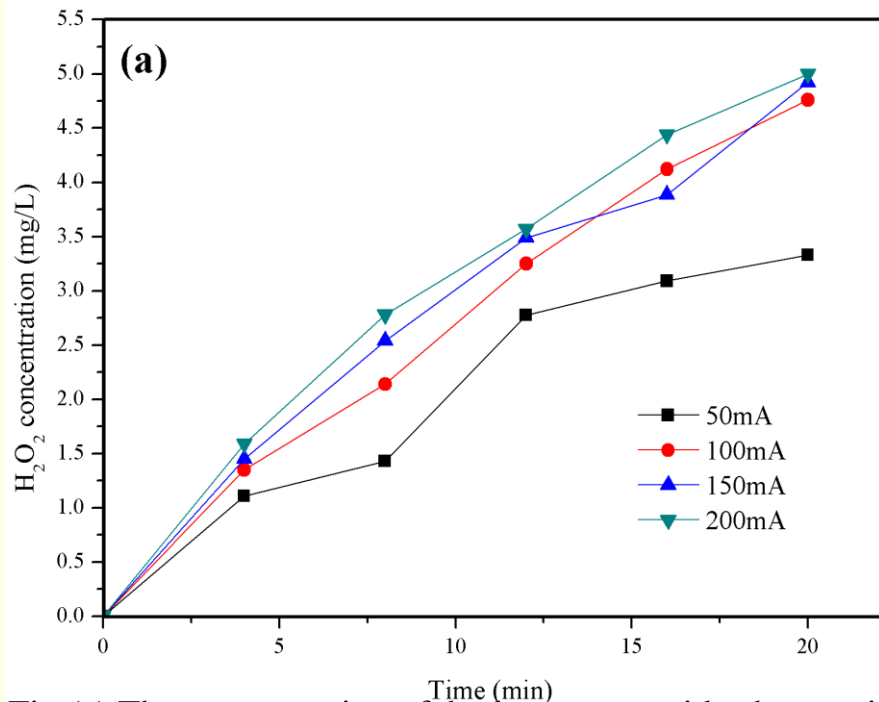


Fig.(a) The concentration of hydrogen peroxide changes in E-ACF system

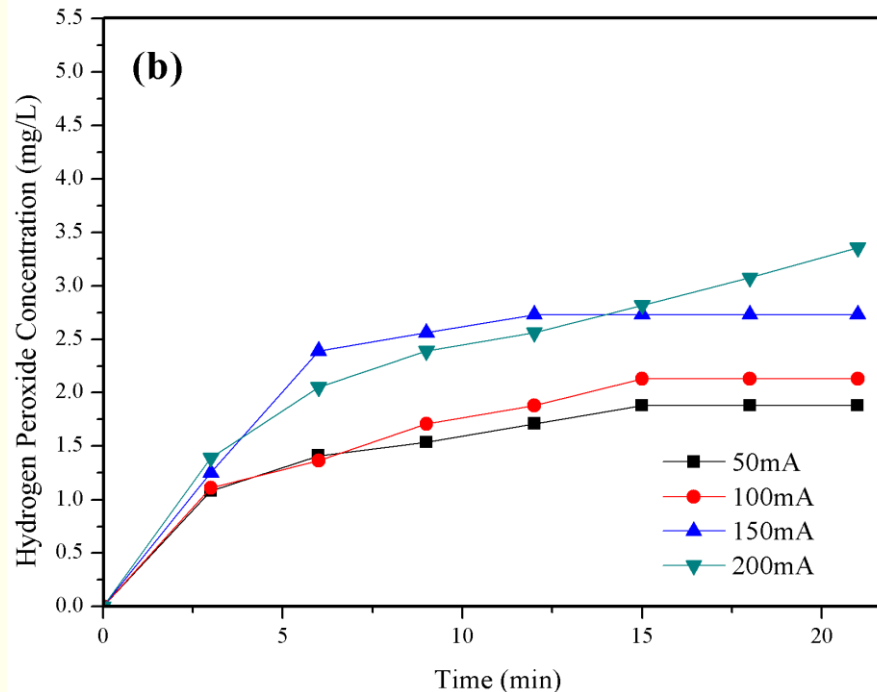


Fig.(b) The concentration of hydrogen peroxide changes in E-peroxone-ACF system

**The hydrogen peroxide which generates in the E-peroxone-ACF system is consumed by ozone, and generate hydroxyl radical which can react with NB.**

# Result and discussion

## Effect of radical scavenger

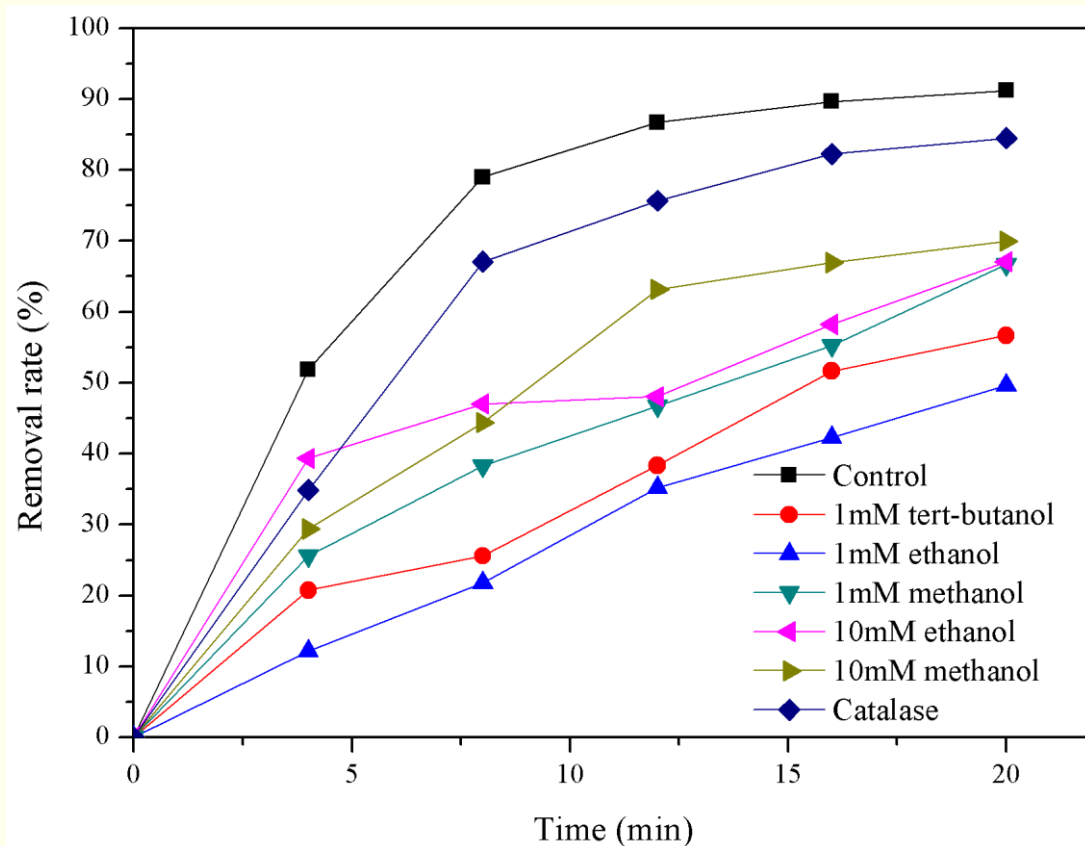


Fig. Effect of radical scavenger on E-peroxone-ACF system

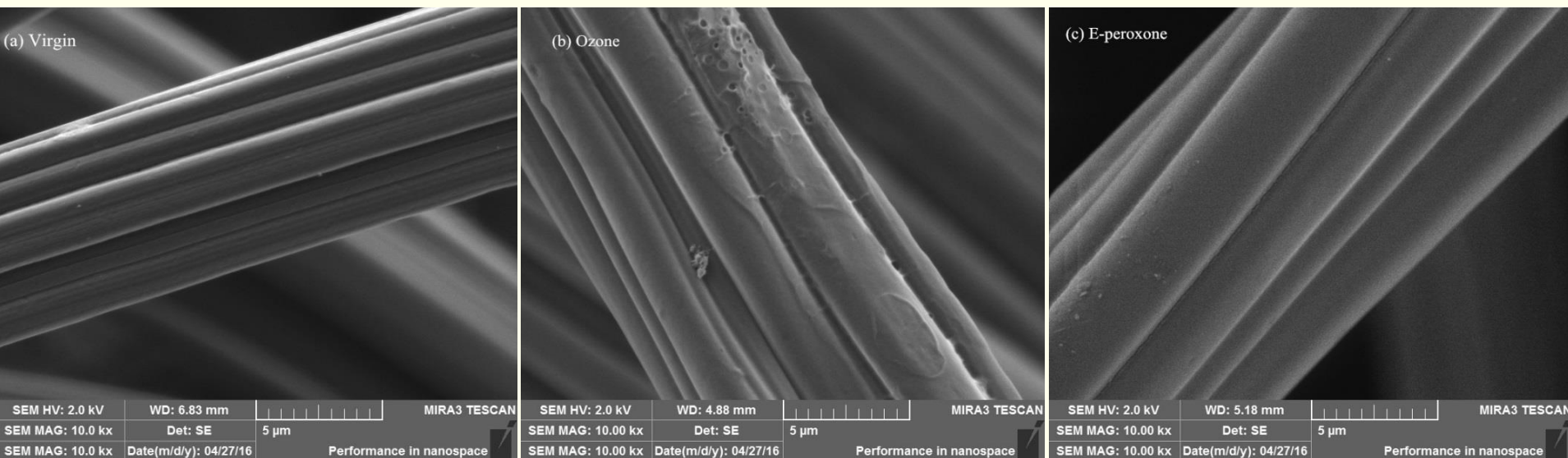
The removal rate decreased rapidly by added 1 mmol/L radical scavenger (methanol, ethanol or TBA) in E-peroxone-ACF system.

**OH radical is the main oxidant!**



# Result and discussion

## The effect of reaction to the surface of ACF



ACF<sub>Virgin</sub>

ACF react with O<sub>3</sub>  
for 100 times  
( O<sub>3</sub>/ACF )

ACF react with O<sub>3</sub> for 100  
times under the protect of  
cathodic electric field  
(E-peroxone-ACF)

**Cathodic electric field can protect ACF to avoid the destruction of ACF surface in ozonation.**

# Result and discussion

## Effects of reaction to the surface structure and functional groups of ACF

Table Comparison of the surface properties and three kinds of ACF

| ACF Sample           | $S_{\text{BET}}$<br>( $\text{m}^2/\text{g}$ ) | $S_{\text{micropore}}$<br>( $\text{m}^2/\text{g}$ ) | $V_{\text{micropore}}$<br>( $\text{m}^3/\text{g}$ ) | $V_{\text{total}}$<br>( $\text{m}^3/\text{g}$ ) | Acidic functional groups<br>( $\mu\text{mole}/\text{g}$ ) | Basic functional groups<br>( $\mu\text{mole}/\text{g}$ ) |
|----------------------|---|---|---|---|---|--|
| ACF <sub>vigin</sub> | 697.44  | 663.52  | 0.287   | 0.331   | 376   | 477  |
| ACF <sub>O3</sub>    | 587.00  | 504.25  | 0.217   | 0.278   | 553   | 187  |
| ACF <sub>E-O3</sub>  | 671.67  | 634.32  | 0.239   | 0.320   | 358   | 504  |

**E-peroxone-ACF process does not alter the surface morphologies and the acidic/basic functional groups of ACF after long time service.**

# Result and discussion

## Effects of reaction to the surface structure and functional groups of ACF

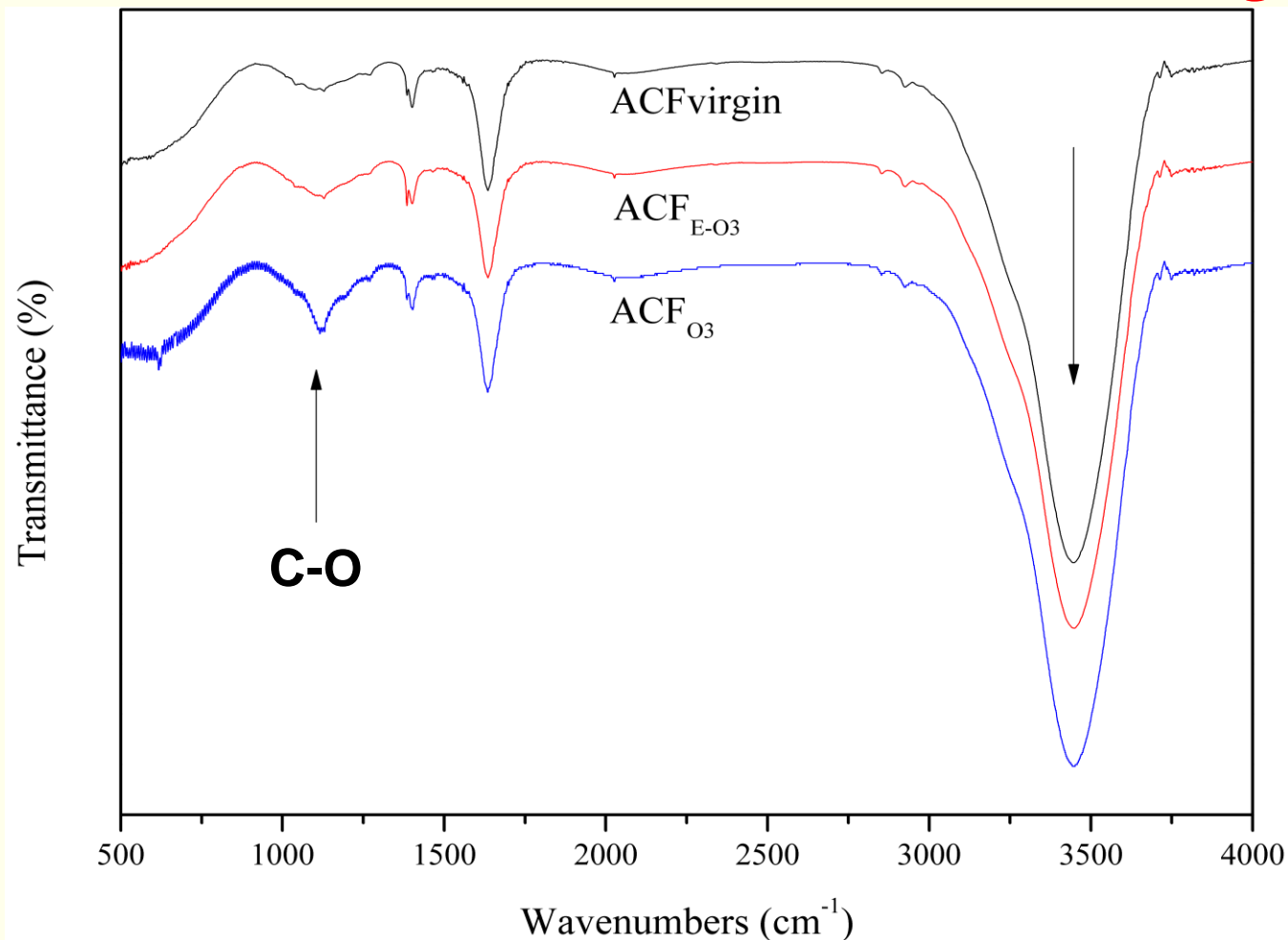
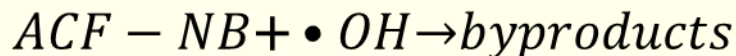
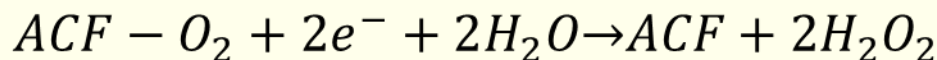
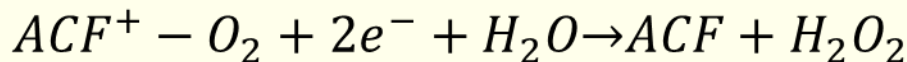
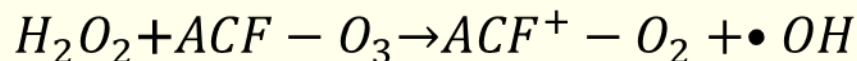
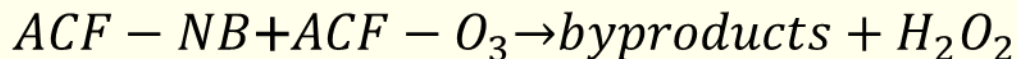
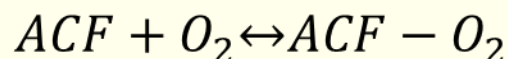
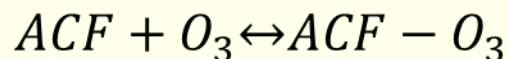
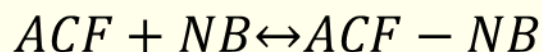


Fig. FTIR of ACF<sub>virgin</sub>, ACF reacted with O<sub>3</sub>, ACF reacted in E-O<sub>3</sub> after 100 times recycle

# Result and discussion

## Reaction mechanism:



**ACF was induced from an initiator/a promoter into an electrocatalyst in ozonation by free electrons injection.**

# Summary

- **EOA process can enhance the removal efficiency of refractory organic contaminations.**
- **Cathodic electric field can protect ACF to avoid ozone oxidation to destroy the surface of ACF.**
- **ACF can be regenerated in situ in the EOA process.**
- **The cathodic ACF combined with ozone can provide effective and sustainable approach to water treatment.**

# Extended research based on persulfate

## E-persulfate-ACF

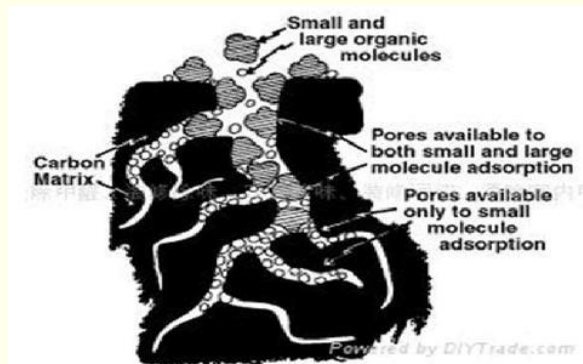
### Direct reaction:

pollutants +  $S_2O_8^{2-}$  ( $E_0=2.01V$ )  $\rightarrow$  product or intermediate products; only for few organic compounds: such as BTEX.

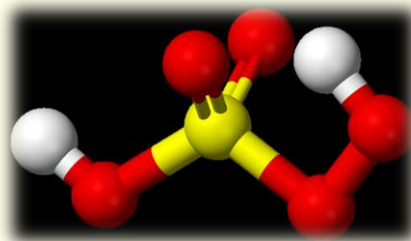
### Indirect reaction:

pollutants +  $SO_4^{\cdot-}$   $\rightarrow$  product or intermediate products;  
for unsaturated hydrocarbon and organic compounds containing benzene ;  $SO_4^{\cdot-}$   
( $E_0=2.60V$ ), high react speed, high potential; low cost

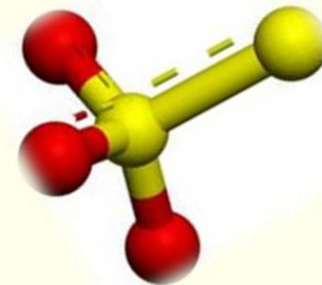
## Activated carbon activation:



+



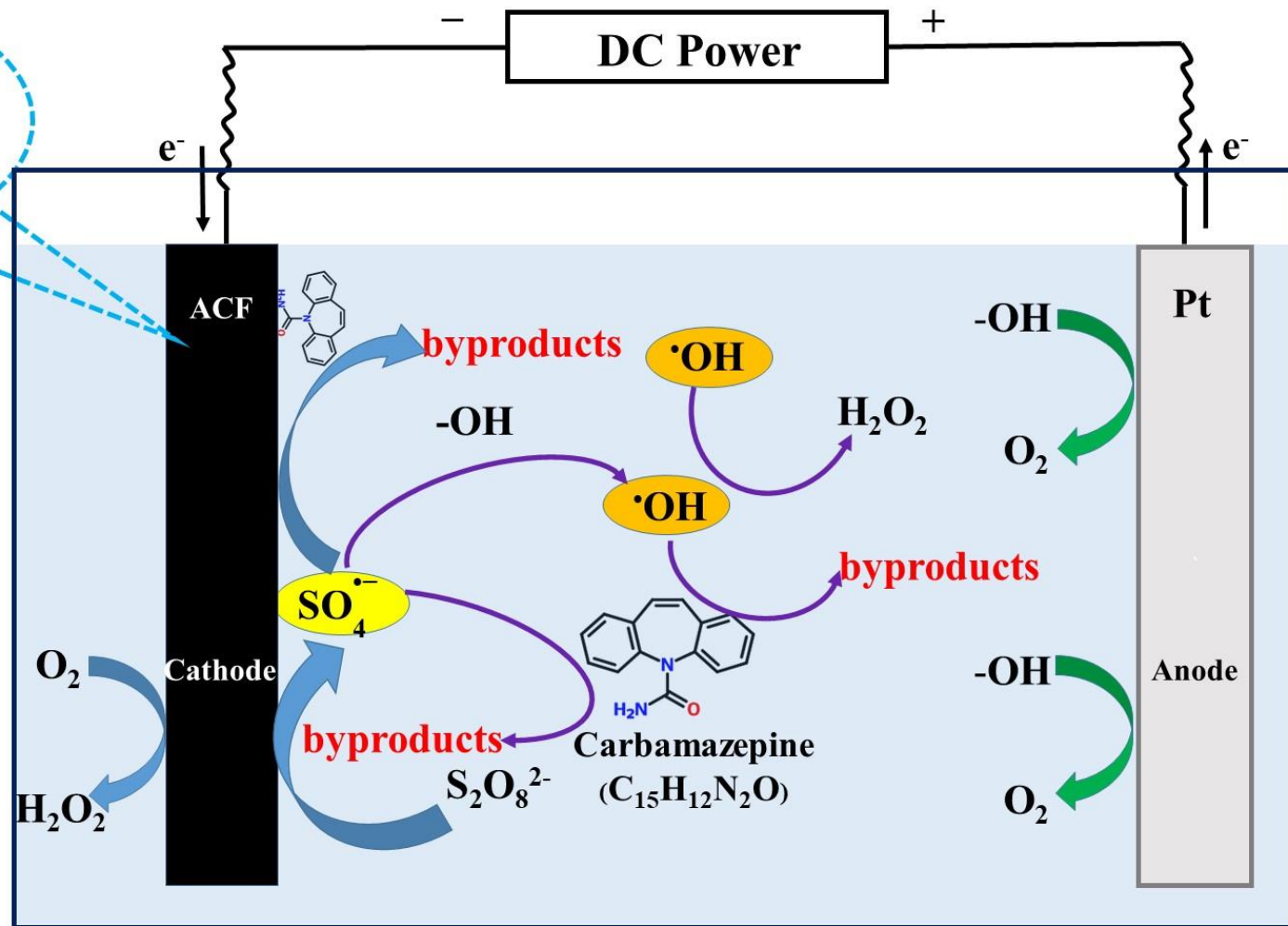
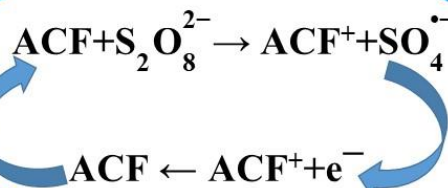
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# Extended research based on persulfate

## Free electron injection on carbon based cathode:



## Electro-persulfate-ACF (E-PS-ACF) process

# Extended research based on persulfate

## E-PS-ACF applied for Carbamapine (CBZ) degradation

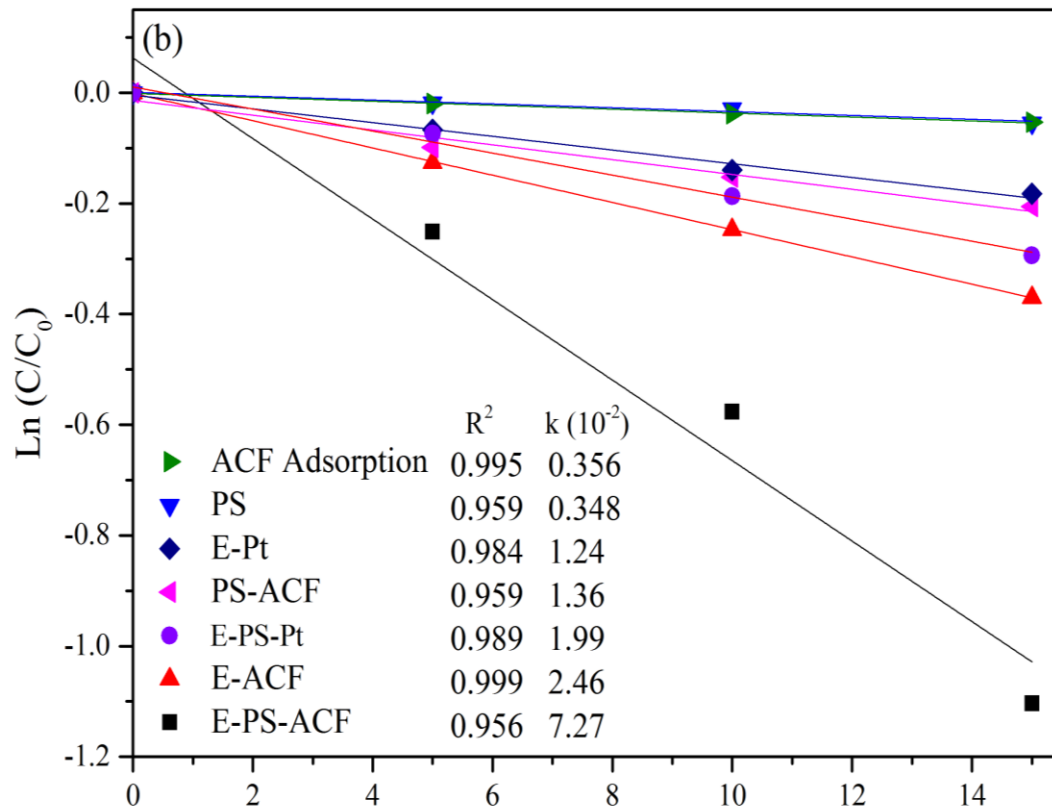


Fig. Reaction kinetics of CBZ removal

1. All processes follow first-order kinetics. The removal efficiency of E-PS-ACF is much higher than the others.

2. CBZ can hardly be removed by PS alone and electricity alone.

3. **There is a coupling effect between persulfate, ACF, and electrolysis.**

# Extended research based on persulfate

## E-PS-ACF

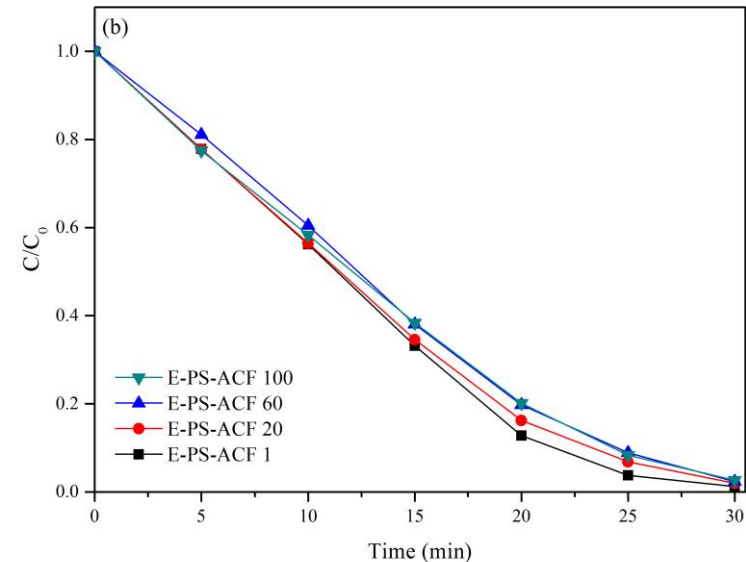
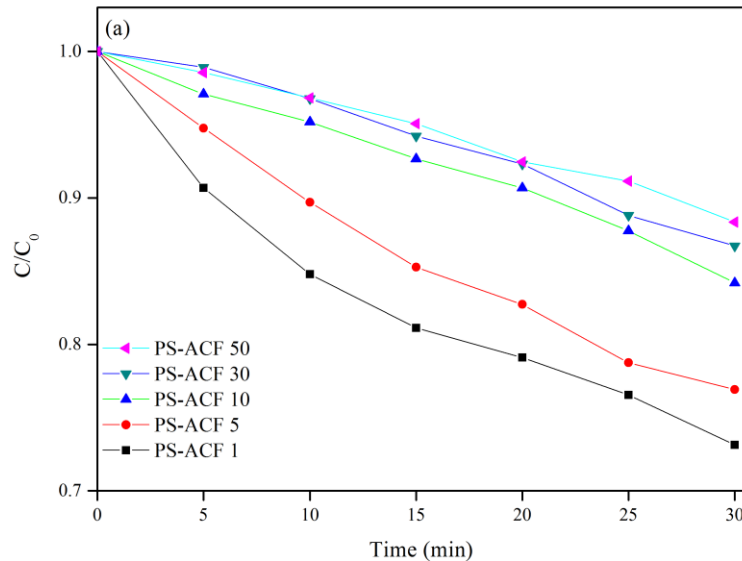


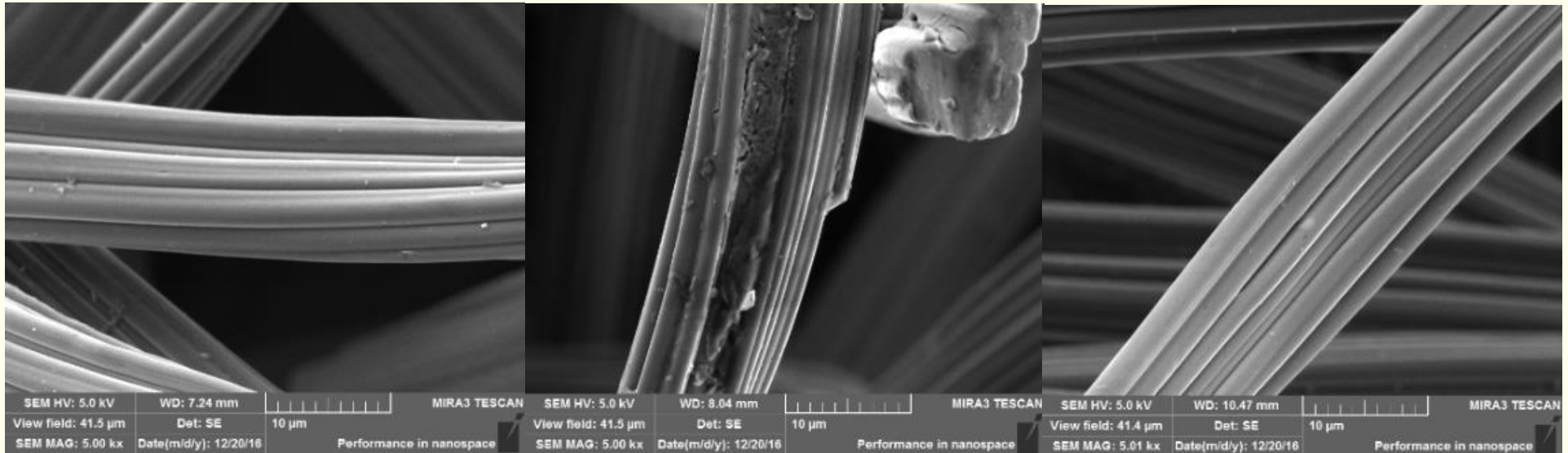
Fig. (a) Degradation of CBZ by PS-ACF process with ACF recycled for 50 times

Fig. (b) Degradation of CBZ by E-PS-ACF process with ACF recycled for 100 times

1. With the increase of ACF recycle times, the removal efficiency of CBZ decreases gradually in PS-ACF system.
2. **With the increase of ACF recycle times, the removal efficiency of CBZ almost unchanged in E-PS-ACF system.**

# Extended research based on persulfate

## E-PS-ACF



ACF<sub>virgin</sub>

ACF<sub>PS-ACF50</sub>

ACF<sub>E-PS-ACF100</sub>

**Cathodic electric field can protect ACF to avoid persulfate oxidation or destroy the surface of the ACF.**

# Extended research based on persulfate

## E-PS-ACF

Table Comparison of the pore texture properties and surface groups of ACF

| Sample                 | $S_{\text{BET}}$<br>( $\text{m}^2 \cdot \text{g}^{-1}$ ) | $S_{\text{micropore}}$<br>( $\text{m}^2 \cdot \text{g}^{-1}$ ) | $V_{\text{micropore}}$<br>( $\text{cm}^3 \cdot \text{g}^{-1}$ ) | $V_{\text{total}}$<br>( $\text{cm}^3 \cdot \text{g}^{-1}$ ) | acidic<br>functional<br>groups<br>( $\mu\text{mol} \cdot \text{g}^{-1}$ ) | Basic functional<br>groups<br>( $\mu\text{mol} \cdot \text{g}^{-1}$ ) |
|------------------------|--|--|---|---|---|---|
| ACF <sub>virgin</sub>  | 624.46   | 557.71   | 0.259   | 0.291   | 408   | 505   |
| ACF <sub>E-PS100</sub> | 589.38   | 525.66   | 0.243   | 0.276   | 389   | 534   |
| ACF <sub>PS50</sub>    | 376.48   | 330.42   | 0.154   | 0.180   | 595   | 355   |

ACFE-PS100 was the ACF reacting in E-PS-ACF system for 100 times.

ACFPS50 was the ACF reacting in PS-ACF system for 50 times.

**E-PS-ACF process does not alter the surface morphologies, BET, and acidic-basic functional group of ACF after long times recycle.**

# Extended research based on persulfate

## E-PS-ACF

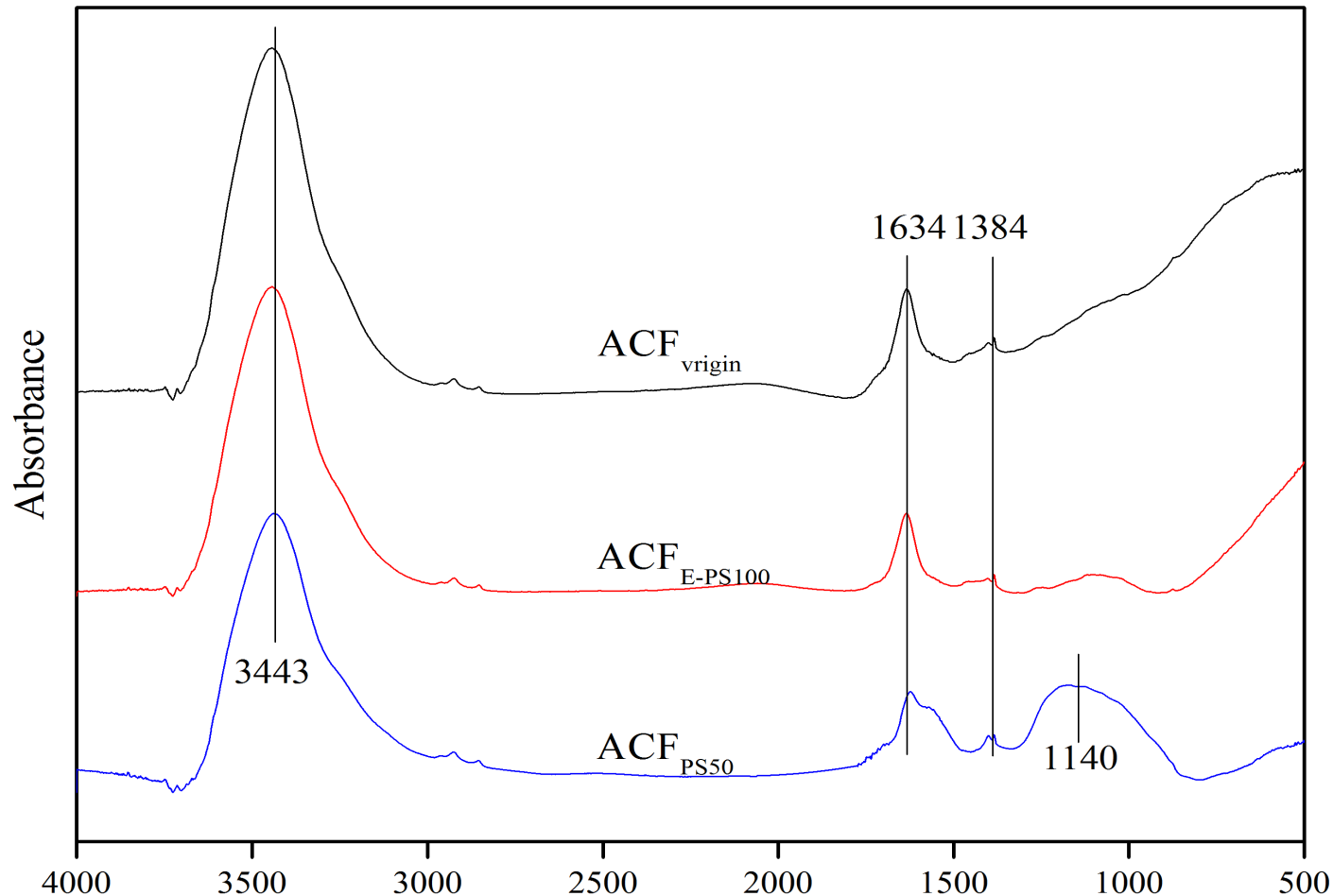


Fig. FTIR of ACF<sub>virgin</sub>, ACF reacted with persulfate (PS-ACF), ACF reacted in E-persulfate (E-PS-ACF).

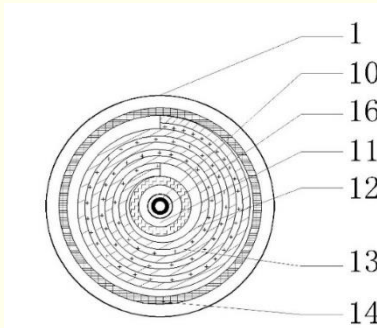
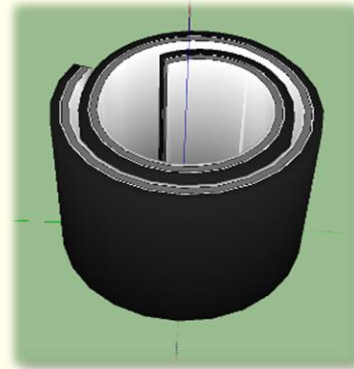


# Reactor Development

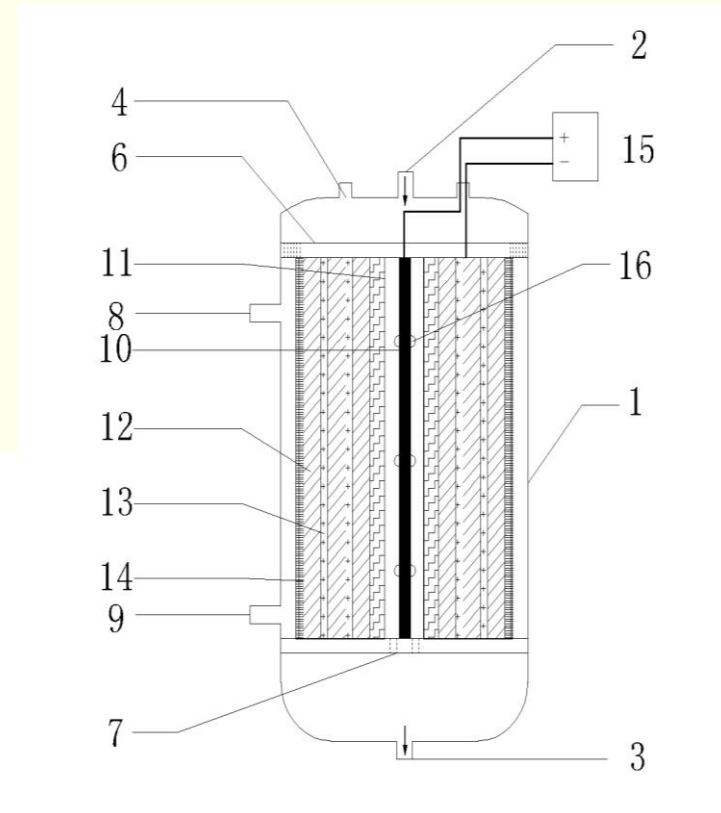
## A spiral electrochemical reactor

The reactor consists of a cylindrical shell, an inlet/port, an outlet/port, and a winding electrode assembly inside the shell.

When the reactor is electrified with oxidants, such as **ozone** and/or **persulfate**, it can produce **hydroxyl radical** and **sulfate radical**. Most organic pollutants are **filtrated**, **adsorbed**, and **degraded** by the **cathodic membrane** from the raw water.



Top View



Perspective Drawing

注：装置壳体（1），进水口（2），出水口（3），出气口（4），接线口（5），布水板（6），过水孔（7），进液口（8），进气口（9），阳极电极层（10），阴阳电极隔绝层（11），阴极电极层（膜过滤层）（12），膜支撑层（13），紧固层（14），直流电源（15），紧固丝（16）

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**Thanks for your attention!**